Comparing different numerical methods for 2D-coupled water and solute transport in porous media

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Context of research

- Comparison of three 2D coupled models for water and solute transport in porous media (1) COMSOL (2) FAESOR and (3) FDM-MIC model.
- Description of 2D FEM for coupled water and solute transport in porous media using FAESOR (Krysl, 2000).
- Description of 2D FDM for water flow coupled with Marker in Cell (MIC) by Gerya (2010), for solute transport in porous media.
- Model verification problems and a application problem → Comparison based on global mass balances, iteration methods, time stepping methods.



Equations Involved - Water Transport

• Richard's Equation

$$\frac{C_m(\Psi^{(a+1,b)}) + S_w S_s}{\Delta t} \delta^{b+1} + \nabla \cdot q = 0 \dots Eq(1,a) \dots Head Based \dots COMSOL$$

$$\frac{\theta^{a+1} - \theta^a}{\Delta t} + \frac{C_m(\Psi^{(a+1,b)}) + S_w S_s}{\Delta t} \delta^{b+1} + \nabla \cdot q = 0 \dots Eq(1,b). Mixed Based \cdot FAESOR/FDM$$

$$\delta^{b+1} = (\Psi^{a+1,b+1} - \Psi^{a+1,b}) \dots Eq(2) \qquad q = -K(\Psi) \nabla (\Psi + z) \dots Eq(3)$$

• van Genuchten functions

$$\boldsymbol{K}(\Psi) = \boldsymbol{k}_r \boldsymbol{K}_{sat} \dots \boldsymbol{E} \boldsymbol{q}(4) \qquad \qquad \boldsymbol{S}_{eff} = [1 + \alpha |\Psi|^n]^{-m} \dots \boldsymbol{E} \boldsymbol{q}(5)$$

$$\begin{split} \theta(\Psi) &= \theta_r + S_{eff}(\theta_s - \theta_r) \dots Eq(6) \qquad k_r = S_{eff}^{1/2} [1 - (1 - S_{eff}^{1/m})^m]^2 \dots Eq(7) \\ S_w &= S_{eff} + \frac{\theta_r}{\theta_s} \dots Eq(8) \qquad \qquad C_m = \frac{\alpha m}{1 - m} (\theta_s - \theta_r) S_{eff}^{1/m} (1 - S_{eff}^{(1/m)})^m \dots Eq(9) \end{split}$$



Equations Involved - Solute Transport

Advection Dispersion Equation

$$\frac{\partial \Theta c}{\partial t} + \nabla \cdot \boldsymbol{u} = 0 \dots Eq(10)$$

$$\boldsymbol{u} = -\boldsymbol{D} \nabla c + \boldsymbol{q} c \dots E \boldsymbol{q} (11)$$

$$D_{\alpha\beta} = \alpha_T [v] \delta_{\alpha\beta} + (\alpha_L - \alpha_T) \frac{v_{\alpha} v_{\beta}}{[v]} + D_m \delta_{\alpha\beta} \dots Eq(12)$$

$$v = \frac{q}{\theta} \dots Eq(13)$$



Initial and Boundary Conditions

Water and	Initial Condition	Boundary Conditions		
Solute Transport Model		top horizontal edge	bottom horizontal edge	
		Neumann	Robbins	
Richards Equation	$\Psi(x, z, 0) = z - z_{ref}$	$\boldsymbol{q}(x,0,t) = \boldsymbol{q}_{top}$	$\boldsymbol{q}(x,-1,t) = -K_{surf}(\Psi_{amb} - \Psi)$	
Advection		Dirichlet	Robbins	
Dispersion Equation	$c(x, z, 0) = c_{ini}$	$c(x, 0, t) = c_{top}$	$c(x,-1,t) = \mathbf{q} c$	



FEM - COMSOL and FAESOR





FAESOR - Richards Equation

- Head based form of RE $C \frac{\partial \psi}{\partial t} \nabla \cdot \mathbf{K} [\nabla(\psi + z)] = 0$
- Applying weighted residual, Green theorem, boundary conditions

$$\int_{v} \eta C \frac{\partial \psi}{\partial t} dV + \int_{v} (\nabla \eta) \cdot \mathbf{K} [\nabla (\psi + z)] dV + \int_{S_{2}} \eta \bar{q}_{n} dS + \int_{S_{3}} \eta K_{surf} (\psi - \psi_{amb}) dS = 0$$

• Solution technique for RE with Picards iteration's scheme (Celia et al, 1990)

$$\boldsymbol{T}_{v}^{b} + \boldsymbol{C}_{m} \frac{\boldsymbol{\delta}_{v}^{b+1}}{\Delta t} + (\boldsymbol{K}_{m} + \boldsymbol{H}_{m}) \boldsymbol{\Psi}_{v} - \boldsymbol{L}\boldsymbol{w}_{v} = 0$$

•
$$\Psi_{v}^{a+1,b+1} = \delta_{v}^{b+1} + \Psi_{v}^{a+1,b}$$

FAESOR - Richards Equation

• Temporal discretization $dt = min(\Delta titer || \Delta t_{max})$

• For convergence $\Psi_{v_{prime}}^{a+1,b+1} = \frac{\Psi_{v}^{a+1,b+1} - \Psi_{v}^{a+1,b}}{dt}$

- Truncation error $truncerr = \frac{\left(\Psi_{v_{prime}}^{a+1,b+1} \Psi_{v_{prime}}^{a+1,b}\right)dt}{2}$
- We have considered $\delta_r = 1 \times 10^{-3}$ and $\delta_a = 1 \times 10^{-3}$ for $convcrit = \delta_r |\Psi_v^{a+1,b+1}| + \delta_a$ and $testval = |\delta_v^{b+1}| - convcrit$
- Loop for convergence with iterations and automatic time stepping *if niter* \geq *maxiter*(*i.e.*25), $\rightarrow \Delta t_{iter} = \Delta t \cdot \mu_1(i.e.0.25) \rightarrow not converged \rightarrow niter = niter+1$

if niter
$$\leq$$
 miniter $(i.e.15)$, $\rightarrow \Delta t_{iter} = \Delta t \cdot mu_2(i.e.1.1)$

 $max(testval) < 0, \rightarrow t = t + \Delta t \rightarrow converged$

FAESOR - Advection Dispersion Equation

- Head based form of ADE $\theta \frac{\partial c}{\partial t} \nabla \cdot \boldsymbol{D}[\nabla(c) \boldsymbol{q} \, c] = 0$
- Applying weighted residual, Green theorem, boundary conditions.

$$\int_{v} \eta \theta \frac{\partial c}{\partial t} dV + \int_{v} (\nabla \eta) \cdot \boldsymbol{D} [\nabla(c) - \boldsymbol{q} c] dV + \int_{S_{3}} \eta n \boldsymbol{q} c dS = 0$$

• Solution technique for ADE with Euler backward (Implicit) method.

$$\left[\frac{1}{\Delta t}\boldsymbol{T}_{v} + \boldsymbol{D}\boldsymbol{A}_{m}\right]\boldsymbol{C}\boldsymbol{o}\boldsymbol{n}_{v_{a+1}} = \left[\frac{1}{\Delta t}\boldsymbol{T}_{v}\right]\boldsymbol{C}\boldsymbol{o}\boldsymbol{n}_{m_{a}} + \boldsymbol{L}\boldsymbol{s}_{v_{a+1}} = 0$$

FDM - Richards Equation

$$\frac{\theta_{ij}^{a+1} - \theta_{ij}^{a}}{\Delta t} + \frac{C_m(\Psi_{ij}^{(a+1,b)}) + S_w S_s}{\Delta t} \delta_{ij}^{b+1} = -\frac{q z_{i+1/2,j} - q z_{i-1/2,j}}{\Delta z_{i-1/2,j}} - \frac{q x_{i,j+1/2} - q x_{i,j-1/2}}{\Delta x_{i,j-1/2}}$$







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Marker-in-Cell

• Eulerian and Lagrangian time derivative of concentration related together by advection term

$$\frac{Dc}{Dt} = \frac{\partial c}{\partial t} + \boldsymbol{q} \cdot \nabla c$$

• Lagrangian term solved on Euler nodes

$$\frac{Dc}{Dt} = -\nabla \cdot \boldsymbol{D} \nabla c$$

• Advection term solved on Lagrangian markers

$$x_{mrk}^{tx_{mrk}+\Delta tx_{mrk}} = x_{mrk}^{tx_{mrk}} + vx_{mrk} \Delta tx_{mrk}$$
$$z_{mrk}^{tz_{mrk}+\Delta tz_{mrk}} = z_{mrk}^{tx_{mrk}} + zx_{mrk} \Delta tz_{mrk}$$







Marker-in-Cell

- Dispersion term on Euler Nodes
- Changes in effective concentration field on Euler nodes
- New marker concentration $c_m^{t+\Delta t} = c_m^t + \Delta c_m$
- Incremental update creates small scale variation on sub-grid, which can be damped by sub-grid diffusion operation
- Subgrid diffusion applied on markers over characteristic local concentration diffusion time scale $\Delta c_m^{subgrid} = c_{m(nodes)}^t - c_m^t \left[1 - \exp\left(-d \frac{\Delta t}{\Delta t_{diff}}\right) \right]$

where
$$\Delta t_{diff} = \frac{1}{2 D_{mx} / \Delta x^2 + 2 D_{mz} / \Delta z^2}$$

•
$$\Delta c_{i,j}^{remaining} = \Delta c_{i,j} - \Delta c_{i,j}^{subgrid}$$

 $c_{m(corrected)}^{t+\Delta t} = c_{m}^{t} + \Delta c_{m}^{subgrid} + \Delta c_{m}^{remaining}$

$$\nabla \cdot \mathbf{D} \nabla c = \frac{-\left(-Dz_{i+1/2,j} \frac{c_{i+1,j} - c_{i,j}}{\Delta z_{i,j}}\right) - \left(-Dz_{i-1/2,j} \frac{c_{i,j} - c_{i-1,j}}{\Delta z_{i-1,j}}\right)}{-\left(-Dx_{i,j+1/2} \frac{c_{i,j+1} - c_{i,j}}{\Delta x_{i,j}}\right) - \left(-Dx_{i,j-1/2} \frac{c_{i,j} - c_{i,j-1}}{\Delta x_{i,j-1}}\right)}{\Delta x_{i,j-1/2}}$$

 $\Delta c_{i,j} = c_{i,j}^{t+\Delta t} - c_{i,j}^{t}$

$$\Delta c_{i,j} = \Delta c_{i,j}^{subgrid} + \Delta c_{i,j}^{remaining}$$

Mass Balance Check

• Water transport *MB*(*t*)= *Total additional mass inside domain*— *Total net flow out of domain* FEM - COMSOL and FAESOR

 $MB_{w}(t) = \sum \left(\theta - \theta_{0}\right) dv - \left[\sum \left(-qx_{in} dz_{i} - qx_{out} dz_{out}\right) + \sum \left(-qz_{in} dx_{in} - qz_{out} dx_{out}\right)\right] dt$

• FDM

 $MB_{w}(t) = \sum \left(\theta - \theta_{0}\right) dv - \left[\sum \left(-qx_{in}\Delta zIN - qx_{out}\Delta zIN\right) + \sum \left(-qz_{in}\Delta xIN - qz_{out}\Delta xIN\right)\right] dt$

• Solute transport

MB(t) = Total additional concentration mass inside domain - Total net flux out of domain

• FEM - COMSOL and FAESOR

$$MB_{s}(t) = \sum \left(\theta c - \theta_{0} c\right) dv - \left[\sum \left(-ux_{in} dz_{in} - ux_{out} dz_{out}\right) + \sum \left(-uz_{in} dx_{in} - uz_{out} dx_{out}\right)\right] dt$$

• MIC

- Dispersion $MB_{sD}(t) = \sum (\theta c - \theta_0 c) dv - \left[\sum (-uDx_{in} \Delta zIN - uDx_{out} \Delta zIN) + \sum (-uDz_{in} \Delta xIN - uDz_{out} \Delta xIN) \right] dt$ $uDx = D_{xx} \frac{dc}{dx} \quad uDz = D_{zz} \frac{dc}{dz}$
- Advection

$$m_{outA} = \sum m_c - m_{recycled}$$
 (Sun, 1999)

Spatial Scenarios: Model Verification



Hydraulic parameters	α [1/m]	n	Θ_{s} [m ³ /m ³]	$\Theta_{r}[m^{3}/m^{3}]$	K _{sat} [m/s]
coarse sand	2.00	1.50	0.40	0.04	5.00 x 10 ⁻²

Material Properties : Model Verification

Parameters	Problem 1	Problem 2	Problem 3
$z_{ref}[m]$	0.00	-1.00	-2.00
c_{ini} [kg/m ³]	1.00	1.00	1.00
q_{top} [m/s]	0	0	0
$K_{surf}[1/s]$	5.0 x 10 ⁻²	5.0 x 10 ⁻²	5.0 x 10 ⁻²
$\Psi_{amb}[m]$	-1.00	-1.00	-1.00
c_{top} [kg/m ³]	0.00	0.00	0.00
$S_{s}[kg/m^{2}s^{2}]$	4.00 x 10 ⁻⁶	4.00 x 10 ⁻⁶	4.00 x 10 ⁻⁶
$D_m [m^2/s]$	$1.00 \ge 10^{-10}$	$1.00 \ge 10^{-10}$	1.00 x 10 ⁻¹⁰
α_L [m]	0.10	0.10	0.10
$\alpha_{T}[m]$	1.0 x 10 ⁻²	1.0 x 10 ⁻²	1.0 x 10 ⁻²





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Figure: Problem 1, $z_{ref} = 0m$, pressure head along depth (• for COMSOL, for FAESOR, \blacktriangle for FDM) at time 0, 100, 275, 365s (a), outlet concentration along time (• for COMSOL, • for FAESOR, **A** for MIC) (b), mass balance for water transport (• for COMSOL, ■ for FAESOR, ▲ for FDM) (c) and Mass balance for solute transport (• for COMSOL, • for FAESOR, **A** for Dispersion term in MIC and \blacktriangle for Advection term in MIC) (d).



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Figure: Problem 2, $z_{ref} = -1m$, pressure head along depth (• for COMSOL, for FAESOR, A for FDM) at time 0, 100, 275, 365s (a), outlet concentration along time (• for COMSOL, • for FAESOR, **A** for MIC) (b), mass balance for water transport (• for COMSOL, ■ for FAESOR, ▲ for FDM) (c) and Mass balance for solute transport (• for COMSOL, • for FAESOR, **A** for Dispersion term in MIC and \blacktriangle for Advection term in MIC) (d).

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Spatial Scenarios : Application Problem



Hydraulic parameters	α [1/m]	n	Θ_{s} [m ³ /m ³]	$\Theta_{r}[m^{3}/m^{3}]$	K _{sat} [m/s]
coarse sand	2.00	1.50	0.40	0.04	5.00 x 10 ⁻²
fine clay	1.00	2.50	0.45	0.08	5.00 x 10 ⁻⁵

Material Properties: Application Problem

Parameters	Application Problem		
$z_{ref}[m]$	-2.00		
c_{ini} [kg/m ³]	1.00		
q_{top} [m/s]	-5.0 x 10 ⁻³		
$K_{surf}[1/s]$	5.0 x 10 ⁻²		
$\Psi_{amb}[m]$	-1.00		
c_{top} [kg/m ³]	0.00		
S_s [kg/m ² s ²]	4.00 x 10 ⁻⁶		
$D_m [m^2/s]$	1.00 x 10 ⁻¹⁰		
$\alpha_L [m]$	0.10		
$\alpha_T[m]$	1.0 x 10 ⁻²		







Figure: Pressure head along depth at time 0,5,25,85,100,250,365s for COMSOL (a), FAESOR (b) and FDM (c). Outlet concentration along Time for COMSOL(d), FAESOR (e), and MIC (f).

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Results: Application Problem



Figure: Mass balances for water and solute transport models for different numerical methods





Results: Application Problem

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Discussions

- In FEM
 - larger amount of test functions reduces residual error thus numerical approximation becomes more accurate. FAESOR (secondary nodes) better results than COMSOL (default primary nodes).
 - COMSOL (Richards Equation is default head based) $\rightarrow \frac{\theta^{(a+1)} \theta^{(a+1)}}{\Delta t} \neq C \frac{\Psi^{a+1} \Psi^{a}}{\Delta t}$ in FAESOR (Richards equation is mixed based) is linearized using with Picards iteration and thus mass balance is improved.
- In FDM, placement of hydraulic conductivities and computation of darcy's velocities on internodes, gives better results.
- Automatic time stepping methods and time step dependent on iterations improves mass balance



Discussions

- During computation of advection term by conventional Euler method, the concentration front produces negative values. And produces values higher than boundary and initial conditions.
- MIC approach of calculating dispersion term on Euler nodes and advection term on Lagrangian markers reduces this error.
- MIC has better mass balance than other convention Euler based methods, described in this research (i.e. COMSOL and FAESOR).



Conclusions

- FAESOR better than COMSOL considering mass balance
- FDM method for water transport and MIC method for solute transport delivers better performance considering mass balance.
 - Could be used to validate lab and field experiments
 - Disadvantage not applicable for irregular geometry unlike FAESOR or COMSOL



References

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Questions ?



